Experimental and modeling study of salt binding and release by stabilized MSWI fly ash wastes

Today presentation main contributors

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Municipal waste incineration plant



2 HCl + CaO \rightarrow CaCl₂ + H₂O (semi-wet process); 50 kg/T of waste

	MSWI fly ash				
Leaching test X3 dominated by chlored	31-210 ride an	→ 40% d sulph	6 of highly soluble fraction,		
dominated by entor		u Sulph			
Bulk chemistry	Zn	\rightarrow	6 000 ppm		
	Pb	\rightarrow	2 000		
	Cu	\rightarrow	400		
	Cr	\rightarrow	100		
Required stabiliz hydraulic binders	zation k	before d	disposal, essentially through		

Stabilized MSWI fly ash

Bulk chemical composition

CaO	40 % wt Dry Material
SiO ₂	18.5 %
Al ₂ O ₃	7 %
Na ₂ O	1.5 %
K ₂ O	1.7 %
SO ₃	2.5 %
CI	8.5 %



Stabilized MSWI fly ash

> An example of the proportion of the main solid phases

CaCl ₂ Ca(OH) ₂ :H ₂ O	5.5 % wt
Calcite	4.5
CSH 1.5	34.5
Ettringite (AFt)	11.5
Friedel's salt (AFm)	22
Halite	2.5
Sylvite	3.0
Portlandite	6
Quartz	4.5

Stabilized MSWI fly ash

>An idea of the initial pore water chemistry (calculation)

рН	12	
Na	35 500 mg/L	1.5 mol/L
К	47 000 mg/L	1.2 mol/L
Са	16 500 mg/L	0.4 mol/L
SiO ₂	1 mg/L	10 ⁻⁵ mol/L
CI	125 000 mg/L	3.6 mol/L
SO ₄	> 300 mg/L	> 5 10 ⁻³ mol/L

Set-up of the dynamic leaching test





- Renewal at 100 ml/h
- T = 20 C
- Partially open conditions

Soxhlet-like leaching test

Set-up of the dynamic leaching test











II. Modeling approach

III. Application to dynamic leaching test

IV. An overview of disposal facility modeling

Reactive transport code HYTEC

Chemistry

- aqueous chemistry
- dissolution/precipitation of solids
- sorption
- microbiological module

Hydrodynamics

- ID, 2D-cylindrical geometry (REV)
- Advective and diffusive transport

$$\frac{\partial \omega c_i}{\partial t} = \nabla \cdot \left(D_d \nabla c_i - c_i U \right) - \frac{\partial \omega \bar{c}_i}{\partial t}$$

for (un)saturated hydric conditions

- Iocal thermodynamic equilibrium
- kinetics on redox, sorption and solid reactivity

• feedback of chemistry on ω and D_{ϵ}

$$D_e(\omega) = D_e(\omega_0) \left(\frac{\omega - \omega_c}{\omega_0 - \omega_c}\right)^m$$

What's the surface of a porous media





First models used diffuion of salts + global kinetic dissolution of the waste surface

REV modeling



- Elementary Volume Representation of the interface rather than a geometrical surface
- Equilibrium approach, kinetics is diffusion-controlled (in a first step)



Activity correction model

B-dot model

- calibrated for NaCl solution
- for ionic strength \leq 1 2 mol/L
- applicable on a wide range of temperature
- gives access to the details of the aqueous speciation

Helgeson's model

for water activity



Stability of the chloride solid phases vs. pH (HYTEC)





IV. An overview of disposal facility modeling





(variable porosity and Deff)



after leaching







Comparison between experimental and calculated porosity profiles











II. Modeling approach

III. Application to dynamic leaching test

IV. An overview of disposal facility modeling



pH: 2D profile and evolution with time at the point of compliance

Chloride conc.: 2D profile and evolution with time at the point of compliance

Conclusion (methodology)

- The "long-term" evolution of the stabilized MSWI FA waste was not fully addressed, the present calculations are still in progress!
- However, the agreement between model and experimental data is far to be bad both for the release of major element and the mineralogy evolution
- Capability of reactive transport codes to mechanistically link the laboratory tests to site scenarios, and therefore to support performance and environmental impact assessments in a more consistent way

